

THE TEMPERATURE FIELD IN A HOLLOW CYLINDER  
DUE TO A SOURCE MOVING ALONG A HELIX

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We solve the problem of the temperature distribution in a hollow cylinder due to a source moving along a helix on the outer surface with boundary conditions of the second kind. The solution can be used to calculate temperature fields on a computer for various forms of processing materials.

A heat source of length  $2h_0$  and (angular) width  $2\beta$  moves along a helix on the outer surface of an infinitely long hollow cylinder, starting at some time  $t = 0$ . The source intensity  $q(t)$  varies with the time in some way. The initial cylinder temperature is everywhere  $T_0$ . There is no heat transfer to the external medium. The thermophysical parameters are assumed to be constant.

It is required to establish the temperature distribution for  $t > 0$ .

We shall solve the problem in cylindrical coordinates moving with the source. The origin is on the cylinder axis and the initial plane from which the angle  $\varphi$  is measured passes through the middle of the source.

Then the problem can be reduced to the solution of the following equation (in nondimensional variables):

$$\frac{\partial \Theta}{\partial Fo} = \frac{1}{\rho} \cdot \frac{\partial}{\partial \rho} \left( \rho \frac{\partial \Theta}{\partial \rho} \right) + \frac{1}{\rho^2} \frac{\partial^2 \Theta}{\partial \varphi^2} + \frac{\partial^2 \Theta}{\partial \xi^2} + U \frac{\partial \Theta}{\partial \xi} + \Omega \frac{\partial \Theta}{\partial \varphi} \quad (1)$$

with initial and boundary conditions

$$\begin{aligned} \Theta(\rho, \xi, \varphi, 0) &= 0, \\ \frac{\partial \Theta}{\partial \rho} \Big|_{\rho=1} &= \begin{cases} 0 & |\xi| > h, \\ 0 & |\varphi| > \beta \\ K(Fo) & |\varphi| \leq \beta \end{cases} \quad |\xi| \leq h, \\ \frac{\partial \Theta}{\partial \rho} \Big|_{\rho=\rho_0} &= 0, \quad \rho_0 = \frac{R_1}{R_2}. \end{aligned}$$

Equation (1) can be solved by the sequential application of Fourier and Hankel transforms [1-3].

Omitting the intermediate calculations, we can write the solution as

$$\Theta(\rho, \xi, \varphi, Fo) = \frac{1}{\pi} \sum_{n=0}^{\infty} \beta_n \sum_s F_{ns} G_n(sp) \int_0^{Fo} K(Fo - \tau) \cos n(\varphi + \Omega\tau) \exp(-s^2\tau) \Phi(\xi, \tau) d\tau,$$

where

$$\begin{aligned} \beta_n &= \delta_n \frac{\sin n\beta}{n\beta}, \\ \delta_n &= \begin{cases} \frac{1}{2} & n = 0, \\ 1 & n = 1, 2, 3, \dots, \end{cases} \\ G_n &= J_n(sp) Y'_n(sp_0) - Y_n(sp) J'_n(sp_0), \end{aligned}$$

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$$F_{ns} = \frac{2s^2 G_n(s)}{(s^2 - n^2) G_n^2(s) - (s^2 \rho_0^2 - n^2) G_n^2(s \rho_0)},$$

$$\Phi(\xi, \tau) = \operatorname{erf} \left( \frac{h + \xi + U\tau}{2 \sqrt{\tau}} \right) + \operatorname{erf} \left( \frac{h - \xi - U\tau}{2 \sqrt{\tau}} \right).$$

The sum with respect to  $s$  is over all positive roots of the equation

$$G_n'(s) = 0.$$

In particular cases:

- 1) when the angular velocity  $\omega = 0$  ( $\Omega = 0$ ) we obtain the solution for a source moving along the  $z$ -axis over the surface of the cylinder;
- 2) when the linear velocity  $v = 0$  ( $U = 0$ ) we obtain the solution for a source rotating about the axis of the cylinder;
- 3) when  $\beta = \pi$  we obtain the solution for an annular source in motion;
- 4) when  $\omega = v = 0$  ( $\Omega = U = 0$ ) we obtain solutions for fixed sources;
- 5) when  $\beta = \pi$  and  $h = \infty$  we obtain the solution for a cylinder heated over the whole of its outer surface. If  $K(Fo) = K = \text{const}$  in this case we obtain the solution given in [1] for boundary conditions of the second kind.

#### NOTATION

$\theta = T - T_0/T_0$	is the nondimensional temperature;
$T$	is the cylinder temperature;
$T_0$	is the initial cylinder temperature;
$\rho = r/R_2$	is the nondimensional radius;
$R_1, R_2$	are internal and external radii of the cylindrical surfaces;
$\xi = z/R_2$	is the nondimensional coordinate in the direction of the $z$ -axis;
$Fo = (a/R_2^2)t$	is the Fourier number;
$a$	is the coefficient of thermal diffusivity;
$\lambda$	is the thermal conductivity coefficient;
$h = h_0/R_2$	is the nondimensional source length;
$K(Fo) = (R_2/\lambda T_0)q(Fo)$	is the nondimensional intensity of the heat flow;
$J_n(s\rho), Y_n(s\rho)$	is the Bessel function;
$U = (v/a)R_2$	is the nondimensional velocity along $z$ -axis;
$\Omega = (\omega/a)R_2^2$	is the nondimensional angular velocity.

#### LITERATURE CITED

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